Studies on the Extraction of Metal Complexes

VIII. The Extraction of La, Sm, Hf, Th, and U(VI) with Oxine and Cupferron

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Solvent extraction has proved to be an important method for the separation and determination of metals in analytical chemistry. The procedures worked out in that field should be applicable to chemical industry as well as in preparative laboratory work since extraction is a very practical unit operation. With a multistage countercurrent extraction process a practically complete fractionation of materials which are closely related may be obtained.

The importance of solvent extraction led our group to study the extraction of lanthanide and actinide complexes with organic solvents. For this purpose, the following metal ions were chosen: La⁺³ (radius * = 1.15 Å), Sm^{3+} (r = 1.07 Å), Th^{4+} (r = 1.02 Å), Hf^{4+} (r = 0.86 Å) and UO_2^{2+} . As the behavior of these elements to some extent is determined by the ion charges and sizes it might be feasible to predict the behavior of other rare earth metals as of the transuranium elements, e.g. Am^{3+} (r = 1.11 Å) or Pu^{4+} (r = 0.92 Å).

It was further considered as favorable if the distribution of the metals between the two phases could be measured radiometrically; suitable radio-isotopes were available for La (La¹⁴⁰), Sm (Sm¹⁵³), Hf (Hf¹⁸¹), and Th (Th²³⁴, UX₁). Two organic solvents were used, chloroform and hexone (methyl isobutyl ketone). Chloroform is known as a very good solvent for metal chelates and hexone was chosen as representative for oxygen-containing solvents.

The ionic strength in the aqueous phase was kept constant at 0.1 M using $HClO_4$, $NaClO_4$ and NaOH, and all experiments were carried out at 25°C. In the following part the extraction of the oxinates and cupferrates are reported.

^{*} The radii are approximately given in the Pauling scale by comparison with data by Zachariasen 1.

INTERPRETATION OF DATA

Data on metal extraction with complex forming agents (HA) such as dithizone and oxine are usually given in diagrams plotting the per cent metal extracted against the pH for a given reagent concentration. The theoretical understanding of these curves have been based on the following reaction

$$\mathbf{M}^{N+}$$
 (aq) + $N \cdot \mathbf{H}\mathbf{A}$ (org) $\rightleftharpoons \mathbf{M}\mathbf{A}_N$ (org) + $N \cdot \mathbf{H}^+$ (aq)

with the equilibrium constant

$$K = \frac{[\mathrm{MA}_N]_{\mathrm{org}} \cdot [\mathrm{H}^+]^N}{[\mathrm{M}^{N+}] \cdot [\mathrm{HA}]_{\mathrm{org}}^N}$$

This equation is however only valid when the water-soluble M—A complexes

may be neglected.

From the very beginning of our work we looked upon this problem of metal extraction as a stepwise complex formation of M^{N+} with a ligand A^- giving among other complexes MA_n , an uncharged extractable complex MA_N . With the use of radioactive tracers we extended the measurable range of the net distribution ratio of M,

$$q = \frac{[\mathbf{M}]_{\text{total, org}}}{[\mathbf{M}]_{\text{total, ag}}}$$

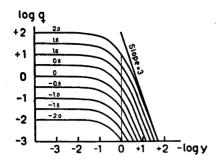
from about 100-0.01 to about 1000-0.001. In doing so we found in most cases that q approached a maximum value (see Fig. 1). This could be explained by assuming the presence of MA_N in the aqueous phase. The distribution constant of this complex is

$$\lambda_N = rac{[\mathrm{MA}_N]_{\mathrm{org}}}{[\mathrm{MA}_N]_{\mathrm{aq}}}$$

Furthermore the data could only be explained if all the complexes MA, MA₂, MA_N were considered. In the mathematical treatment ^{2.3} of our data we have found it most useful to plot $\log q$ against $\log [A^-]$. Calculations on these curves have enabled the more or less independent determination of λ_N and the various complexity products κ_n .

$$\varkappa_n = \frac{[\mathbf{M}\mathbf{A}_n]}{[\mathbf{M}][\mathbf{A}]^n} = k_1 \cdot k_2 \cdot \dots \cdot k_n$$

Most of the experimental data in this work is therefore found in other articles $^{4.5}$. where the complex formation constants and distribution constants are calculated. The log q curves in those papers are here transformed to curves where the ordinate is $100 \cdot q/1 + q$, i.e. per cent metal extracted. Figure 1 shows an evenly spaced family of log q curves with different values of λ_N and how it spreads out around q = 1 in the $100 \cdot q/1 + q$ interpretation. The characteristic type of curves in Figure 6 are obtained when log $\lambda_N \geq 2$.



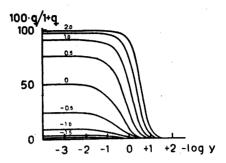
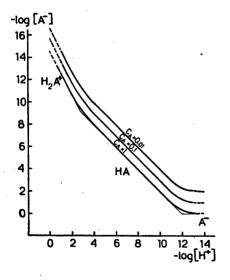


Fig. 1. Variation of the net distribution ratio q in two different graphical representations for various values for the logarithm of the partition coefficient λ_3 of the uncharged complex MA₃. Abscissa: $-\log y = -\log [A] - a$ (cf. part V^3 , the parameter b is 0.25, N = S = 3).

As stated above the abscissa chosen is generally pH while we prefer to use $-\log [A^-]$. With this representation the points for different values of the initial reagent concentration in one phase, C_A , will usually coincide. In Figures 2 and 3 the relations between pH (-log $[H^+]$) and $-\log [A^-]$ for the oxine-chloroform and cupferron-hexone, cupferron-chloroform systems are shown.



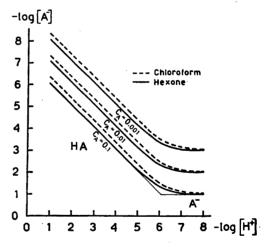


Fig. 2. The oxinate ion concentration (— log [A]) as a function of the hydrogen ion concentration for different values of the initial oxine concentration in the chloroform phase $C_{\mathbf{A}}$ (in moles|lit.). The volume of the aqueous phase is equal to the volume of the organic phase.

Fig. 3. The cupferrate ion concentration (— $\log [A^*]$) as a function of the hydrogen ion concentration for different values of the initial Na-cupferrate concentration in the aqueous phase C_A (in moles|lit.). The volume of the aqueous phase is equal to the volume of the organic phase.

Table 1. Distribution of UO_2^{2+} . The oxine-chloroform system.

Initial conc. of oxine in the CHCl ₃ phase M	Initial cone. of U in the aq. phase M	$rac{100 \cdot q}{1 + q}$	$\log q$	-log [H ⁺]	−log [A⁻]
0.100	0.001	Λ1	(200)	1.91	11.05
0.100		0.1	(-3.00)		11.95
0.100	0.001	0.5	(-2.30)	2.05	11.70
0.100	0.001	2.8	(-1.54)	2.21	11.42
0.100	0.001	. 9.4	-0.98	2.34	11.21
0.100	0.001	32.1	-0.32	2.46	11.03
0.100	0.001	36.2	-0.24	2.48	11.00
0.100	0.001	55.5	+0.11	2.57	10.87
0.100	0.001	57.6	+0.13	2.59	10.84
0.100	0.001	55.5	+0.11	2.68	10.71
0.100	0.001	79.2	+0.59	$\frac{2.71}{2.72}$	10.67
0.100	0.001	85.2	+0.77	2.73	10.64
0.100	0.0001	4.6	(-1.32)	2.23	11.39
0.100	0.0001	16.2	-0.70	$\begin{array}{c} 2.32 \\ 2.46 \end{array}$	11.25
0.100	0.0001	40.4	-0.16		11.03
0.100	0.0001	56.6	+0.11	2.58	10.85
0.100	0.0001	69.2	+0.35	2.59	10.84
0.100	0.0001	77.4	+0.54	2.63	10.78
0.100	0.0001	81.6	+0.65	$\frac{2.67}{2.72}$	10.72
0.100	0.0001	90.5	+0.97	$\frac{2.72}{2.70}$	10.66
0.100	0.0001	94.0	(+1.20)	2.79	10.56
0.100	0.0001	94.5	(+1.24)	$\begin{array}{c} 2.85 \\ 3.53 \end{array}$	10.49
0.100 0.100	0.0001	$\begin{array}{c} 99.0 \\ 84.4 \end{array}$	(+1.99)	10.38	$\begin{array}{c} 9.69 \\ 2.57 \end{array}$
	0.0001		+0.73		
$0.100 \\ 0.100$	$0.0001 \\ 0.0001$	$\begin{array}{c} 77.5 \\ 68.2 \end{array}$	+0.54	10.55 · 10.77	$\begin{array}{c} \textbf{2.41} \\ \textbf{2.20} \end{array}$
0.100	0.0001	58.2	$^{+0.33}_{+0.14}$	10.77	2.20
0.100	0.0001	47.5	-0.05	10.50	2.08 1.84
0.050	0.0001	12.1	-0.86	2.40	11.42
0.050	0.0001	18.8	-0.64	$\begin{array}{c} 2.40 \\ 2.45 \end{array}$	11.42
0.050	0.0001	$\begin{array}{c} 13.3 \\ 22.3 \end{array}$	-0.54	$\begin{array}{c} 2.43 \\ 2.49 \end{array}$	11.29
0.050	0.0001	29.1	$-0.34 \\ -0.39$	$\begin{array}{c} 2.49 \\ 2.53 \end{array}$	11.23
0.050	0.0001	39.3	-0.39 -0.19	$\begin{array}{c} 2.53 \\ 2.59 \end{array}$	11.14
0.050	0.0001	46.6	-0.19 -0.06	$\begin{array}{c} 2.39 \\ 2.71 \end{array}$	10.97
0.050	0.0001	67.9	$-0.00 \\ +0.40$	$\begin{array}{c} 2.71 \\ 2.85 \end{array}$	10.79
0.050	0.0001	72.5	$+0.40 \\ +0.42$	$\begin{array}{c} 2.83 \\ 2.88 \end{array}$	10.75
0.050	0.0001	79.7	$^{+0.42}_{+0.59}$	$\begin{array}{c} 2.88 \\ 2.98 \end{array}$	10.73
0.050	0.0001	83.8	$^{+0.35}_{+0.71}$	3.04	10.54
0.020	0.0001	6.7	(-1.14)	2.69	11.40
0.020	0.0001	6.7	(-1.14)	$\begin{array}{c} 2.05 \\ 2.75 \end{array}$	11.31
0.020	0.0001	10.8	-0.87	$\begin{array}{c} 2.73 \\ 2.79 \end{array}$	11.26
0.020	0.0001	15.9	-0.72	$\begin{array}{c} 2.13 \\ 2.78 \end{array}$	11.27
0.020	0.0001	19.1	-0.63	2.86	11.17
0.020	0.0001	35.3	-0.26	3.04	10.95
0.020	0.0001	53.1	+0.05	3.19	10.77
0.020	0.0001	76.1	+0.51	3.43	10.49
0.020	0.0001	86.5	+0.81	3.54	10.38
0.020	0.0001	86.5	+0.81	3.70	10.22
1 0.020	0.0001		T 0.01	0.10	10.44

Initial conc. of oxine in the CHCl ₃ phase M	Initial conc. of U in the aq. phase M	$rac{100 \cdot q}{1+q}$	$\log q$	log [H+]	-log [A-]
0.100	0.001	4.7	(-1.31)	2.32	11.17
0.100	0.001	12.7	-0.83	2.44	10.97
0.100	0.001	20.2	-0.59	2.53	10.81
0.100	0.001	27.5	-0.41	2.57	10.75
0.100	0.001	37.5	-0.21	2.63	10.65
0.100	0.001	48.8	-0.02	2.65	10.61
0.100	0.001	59.0	+0.16	2.74	10.47
0.100	0.001	66.0	+0.29	2.78	10.40
0.100	0.001	72.5	+0.43	2.82	10.35
0.100	0.001	80.5	+0.62	2.91	10.21
0.100	0.001	83.3	+0.70	2.93	10.17

Table 2. Distribution of UO_2^{2+} . The oxine-hexone system.

These curves are calculated from data given in Part IV of this series ⁶. It is seen from the curves that the same $-\log [A^-]$ value may be obtained for different C_A values simply by changing $-\log [H^+]$ in the aqueous phase. The figures also show that the oxine-chloroform systems has two buffer points at $-\log [H^+]$ 2.72 (p k_1 -log p) and 11.94 (p k_2 + log p) and that the cupferronhexone system has one point at $-\log [H^+]$ 6.09 (p k_a + log p).

Table	3.	Distribution	of	UO_2^{2+} .	The	$cup {\it ferron-chloroform}$	system.
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Initial conc. of Na- cupferrate in the aq. phase M	Initial cone. of U in the the aq. phase M	$rac{100 \cdot q}{1+q}$	q *	—log [H+]	—log [A·]
0.01 0.01 0.01 0.01 0.01 0.01 0.01 0.01 0.01 0.01 0.01 0.01	0.0001 0.0001 0.0001 0.0001 0.0001 0.0001 0.0001 0.0001 0.0001 0.0001	7.3 14.3 24.8 36.1 38.0 35.3 28.2 27.2 27.5 25.6 30.6	0.57 0.61 0.55 0.55 0.39 0.37 0.38 0.34 0.44 0.31	2.42 2.86 3.22 3.58 3.63 3.78 4.01 4.35 4.70 5.14 5.26 5.69 5.88	5.92 5.48 5.12 4.76 4.71 4.56 4.33 3.99 3.65 3.22 3.12 2.76 2.60

^{* 10} q-values chosen for the determination of $q_{max} = \lambda_2 = 0.45$

Initial conc. of Na- cupferrate in the aq. phase M	Initial conc. of U in the aq. phase M	$rac{100 \cdot q}{1+q}$	q *	—log [H+]	—log [A-]
0.01 0.01 0.01 0.01 0.01 0.01 0.01 0.01	0.0001 0.0001 0.0001 0.0001 0.0001 0.0001 0.0001 0.0001	17.5 15.9 42.3 50.9 67.3 82.2 69.0 65.2 50.7 76.8	2.97 4.62 3.29 2.63 1.03 3.31	1.30 1.43 1.84 1.96 2.12 2.36 2.42 2.59 2.61 2.99	6.75 6.62 6.21 6.09 5.93 5.69 5.63 5.46 5.44 5.06
0.01 0.01	$0.0001 \\ 0.0001$	$\begin{array}{c} \textbf{42.5} \\ \textbf{71.1} \end{array}$	$\begin{array}{c} \textbf{0.74} \\ \textbf{2.46} \end{array}$	3.57 5.30	$\begin{array}{c} \textbf{4.48} \\ \textbf{2.82} \end{array}$

Table 4. Distribution of UO₂²⁺. The cupterron-hexone system.

EXPERIMENTAL

All experiments were carried out as described earlier ⁴. The volume of the two phases were equal. Only small amounts of the metals were used and the distribution between the organic and aqueous phases was measured radiometrically in the case of La, Sm, Hf, and Th and spectrophotometrically in the case of U (VI) ⁷. The radioisotopes of La, Sm, and Hf were obtained by neutron irradiation of the corresponding oxides at AERE, Harwell; Th²²⁴ (UX₁) was used as a tracer for Th. It might be pointed out that the metals were not mixed, the experiments being run separately for each metal. The La and Sm data are given in Part XVII ⁵, the Th data have been given in Part VI ⁴ and the data on the uranyl ion are given in Tables 1—4 and in Figures 4 and 5. With Hf very few experiments were carried out and the results are only approximate.

It should be noted that we used no buffers such as phosphate and the pH in the 0.1 M NoCH approximates were reason for this is

It should be noted that we used no buffers such as phosphate and the pH in the 0.1 M NaClO₄ aqueous phase was adjusted with HClO₄ and NaOH. The reason for this is apparent as perchlorate ions are considered not to form metal complexes. Of course it was then somewhat difficult to obtain the right pH between 5 and 9 with the oxine system.

RESULTS

The uranyl-oxine system: Within the small $\log q$ range investigated it is not possible to calculate \varkappa_1 , \varkappa_2 and λ_2 as the points fall on a straight line with a slope equal to 2. From Fig. 4 we may obtain at $\log q = 0$ $\lambda_2 \cdot \varkappa_2 = 10^{2 \cdot 10.94}$ for the chloroform system and $\lambda_2 \cdot \varkappa_2 = 10^{2 \cdot 10.54}$ for hexone (equation 7 in Part V³). Figure 5 gives likewise $\lambda_2 \cdot \varkappa_2 \cdot \varkappa_3^{-1} = 10^{-1.88}$ for chloroform (equation 8 in Part V³). In this way

$$\varkappa_3 = \frac{[\mathrm{UO}_2 \mathrm{A}_3^-]}{[\mathrm{UO}_2^{2+}][\mathrm{A}]^3} = 10^{23.76}$$

is obtained.

^{* 8} q-values chosen for the determination of $q_{\text{max}} = \lambda_2 = 2.63$

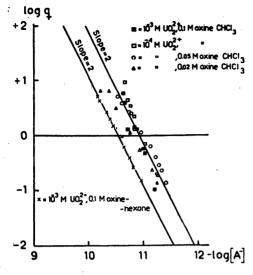


Fig. 4. The distribution of the uranyl ion between chloroform or hexone and acid perchlorate solutions as a function of the oxinate ion concentration $(-\log [A])$.

The oxine-system: The difference between chloroform and hexone as a solvent extraction liquid for oxine or the metal oxinates is very small, chloroform having a slightly better solving capacity. Fig. 6 shows the results with the chloroform-oxine system. It is seen that all of these metals can be extracted at different—log [A] values, thus it is possible to separate them by means of controlled pH. The sequence between Hf⁴⁺, Th⁴⁺, Sm³⁺, and La³⁺ is the one expected from the charges and sizes of the ions, the uranyl ion, however, seems to hold a unique position. It should also be noted that Th and U are re-extracted at high concentration of A (low —log [A] values) probably because negative complexes are formed.

The cupferron system: For the metal cupferrates investigated here hexone is a better solvent, even though cupferron (HA) itself is more soluble in chloroform than hexone (cf. Part IV⁶). The extraction of Hf⁴⁺ and Th⁴⁺ is very good and takes place at low values of $-\log [A^-]$ as seen from Fig. 7. The extraction of La³⁺ and especially UO₂²⁺ is poor, the solubility in the organic

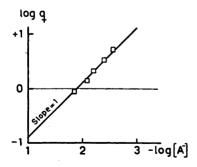
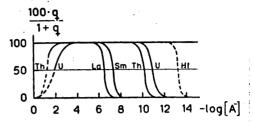


Fig. 5. The distribution of the uranyl ion between chloroform and alkaline perchlorate solutions as a function of the oxinate ion concentration (— log [A]).

Fig. 6. The distribution of La (III), Sm (III), Hf (IV), Th (IV), and U (VI) between chloroform and perchlorate solutions as a function of the oxinate ion concentration $(-\log [A^-])$.



phase being only slightly greater than in the aqueous phase. The sequence between Hf, Th, Sm and La is the same as for oxine, but it may be noted that the position of U in relation to Th has changed. Also in this case it is possible to separate the metals at a controlled pH. However, it should be remembered that cupferron decomposes quite readily.

DISCUSSION

Although oxine and cupferron show excellent possibilities for separating the metals investigated by us, it should be pointed out that the total metal concentration always was low ($<10^{-3}>10^{-8}~M$). If we had used higher metal concentrations the metal oxinates and cupferrates would have precipitated at certain pH values. Some data on the solubilities that we have obtained are given in Table 5 together with Lacroix's 8 values of the Al, Ga and In oxinates.

Feigl ⁹ connects the solubility of the oxinates with their content of bound water or oxine (HA). We are of the same opinion as Pokras, Kilpatrick, and Bernay¹⁰ that H₂O or HA in many cases is bound only by weak lattice for-

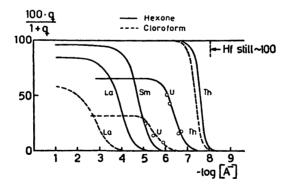


Fig. 7. The distribution of La (III), Sm (III), Hf (IV), Th (IV), and U (VI) between hexone or chloroform and perchlorate solutions as a function of the cupferrate ion concentration (— log [A]). The plateau's for the uranyl curves are calculated from data in Tables 3 and 4.

Solvent / reagent	Metal ion	Temp. °C	Solubility moles / lit
Chloroform (aq.sat.) / oxine Hexone (Th ⁴⁺ Th ⁴⁺ UO ²⁺ Sr ²⁺ Al ³⁺ Ga ³⁺ In ³⁺	25 25 25 25 25 18 18	$ \begin{array}{c} (6.4 \pm 1.7) \cdot 10^{-4} \\ (5.4 \pm 1.0) \cdot 10^{-4} \\ 7.76 \cdot 10^{-4} \\ 0.94 \cdot 10^{-4} \\ 0.045 \\ 0.092 \\ 0.24 \end{array} $
Chloroform (aq.sat.) / cupferron Hexone (») / »	La ³⁺ La ³⁺	25 25	$(5.6 \pm 0.6) \cdot 10^{-4} \ (4 \pm 4) \cdot 10^{-4}$

Table 5. Solubilities of some metal oxinates and cupterrates.

ces. It is therefore questionable if this binding should be connected with the extraction of the metal oxinates. How irregular the H₂O or HA appears is shown by a few examples 9,11:

Precipitates with HA: Sc³⁺, Th⁴⁺, UO₂²⁺

- with 2 H_2O : Mg^{2+} , Mn^{2+} , Ni^{2+} , Cd^{2+} , Ce^{4+} without HA or H_2O : Al^{3+} , Fe^{3+} , Cu^{2+} , La^{3+} , WO_2^{2+}

As pointed out by Moeller 12 the pH of the extraction is closely related to the pH of the precipitation of the metal oxinates. This case may however not be taken as a rule, it should rather be taken as a coincidence of the factors that determine extraction and precipitation.

The pH at which the extraction begins depends on the reagent concentration, $C_{\rm A}$, as seen from Figures 2, 3, 6 and 7. If the reagent concentration is too low the metal ions will be hydrolyzed before the complex formation and extraction with A takes place. With oxine a rather high concentration (0.1-0.5 M) is generally needed and with cupferron much lower concentrations can be used (0.005-0.010 M).

The lanthanides and actinides are of course not the only metals that are extractable as oxinates and cupferrates. Table 6 summarizes data found on oxine-chloroform extraction of different metals. The extraction of cupferrates has been extensively treated by Furman, Mason and Pekola 15 and qualitative data on the extraction of many metal oxinates and cupferrates with chloroform are given by Gorbach and Pohl 16.

SUMMARY

Extraction data on the oxinates and cupferrates of La(III), Sm(III), Hf(IV), Th(IV) and U(VI) are given. Two organic solvents have been used, chloroform and hexone. The ionic strength of the aqueous phase has been kept constant at 0.1 M using HClO₄, NaClO₄ and NaOH, and all experiments were carried out at 25° C. Curves are given showing the partition of the metals

Table 6.	The	pH	for	<i>50</i>	%	extraction	of	metal	oxinates	with	chloroform.
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Metal ion	pH	Procedure	Reference
Ga ³⁺ In ³⁺ Al ³⁺	1.0 2.1 3.4	$V_{ m aq} = V_{ m org}, \; 0.1 \; M \; { m total \; oxine}.$ Anions in aq. sol.: chloride	8 .
Fe ³⁺ Cu ²⁺ In ³⁺ Bi ³⁺ Al ³⁺ Ni ²⁺ Co ²⁺	1.6 2.0 2.2 3.0 4.2 6.1 6.5	4 successive extractions with 0.01 M solution of oxine in chloroform. Anions in aq. sol.: sulfate, acetate, nitrate, chloride	12, 13
$egin{array}{l} \operatorname{Sn}^{4+} & \operatorname{Mo} & \\ \operatorname{Mo} & \operatorname{Fe}^{3+} & \\ \operatorname{Cu} & \operatorname{Ni} & \\ \operatorname{Al} & \operatorname{Mn}^{2+} & \end{array}$	0.0 1.0 2.0 2.1 3.7 3.8 6.4	$V_{ m aq} = 5 \cdot V_{ m org}, \ 0.07 \ M \ m oxine.$ Anions in aq. sol.: acetate, chloride, tartrate	14
Hf^{4+} UO_{2}^{2+} Th^{4+} Sm^{3+} La^{3+}	1.3 * 2.6 3.1 5.7 6.5	$V_{ m aq} = V_{ m org}, \; 0.1 \; M \; { m total \; oxine}.$ Anions in aq. sol.: perchlorate	this work

^{*} $pH = -\log [H^+] + 0.1$

between the organic phase and the aqueous phase as a function of the oxinate or cupferrate ion concentration.

From these curves it is evident that the metals can be separated by extraction with these systems.

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